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# UTILITY PATENT APPLICATION TRANSMITTAL

(Only for new nonprovisional applications under 37 CFR 1.53(b))

Attorney Docket No. 12,150

First Inventor David W. Warren

Thermally-Integrated Low Temperature  
Title WATER-GAS SHIFT REACTOR APPARATUS AND PROCESS

Express Mail Label No.

## APPLICATION ELEMENTS

See MPEP chapter 600 concerning utility patent application contents.

1. ☒ Fee Transmittal Form (e.g., PTO/SB/17)  
(Submit an original and a duplicate for fee processing)
2. ☒ Applicant claims small entity status.  
See 37 CFR 1.27.
3. ☒ Specification [Total Pages 26]  
(preferred arrangement set forth below)
  - Descriptive title of the invention
  - Cross Reference to Related Applications
  - Statement Regarding Fed sponsored R & D
  - Reference to sequence listing, a table, or a computer program listing appendix
  - Background of the Invention
  - Brief Summary of the Invention
  - Brief Description of the Drawings (if filed)
  - Detailed Description
  - Claim(s)
  - Abstract of the Disclosure
4. ☒ Drawing(s) (35 U.S.C. 113) [Total Sheets 4]
5. Oath or Declaration [Total Pages 2]
  - a. ☒ Newly executed (original or copy)
  - b. ☐ Copy from a prior application (37 CFR 1.63 (d))  
(for continuation/divisional with Box 17 completed)
    - i. ☐ DELETION OF INVENTOR(S)  
Signed statement attached deleting inventor(s) named in the prior application, see 37 CFR 1.63(d)(2) and 1.33(b).
6. ☐ Application Data Sheet. See 37 CFR 1.76

ADDRESS TO: Assistant Commissioner for Patents  
Box Patent Application  
Washington, DC 20231

7. ☐ CD-ROM or CD-R in duplicate, large table or Computer Program (Appendix)
8. Nucleotide and/or Amino Acid Sequence Submission (if applicable, all necessary)
  - a. ☐ Computer Readable Form (CRF)
  - b. Specification Sequence Listing on:
    - i. ☐ CD-ROM or CD-R (2 copies); or
    - ii. ☐ paper
  - c. ☐ Statements verifying identity of above copies

## ACCOMPANYING APPLICATION PARTS

9. ☒ Assignment Papers (cover sheet & document(s))
10. ☐ 37 CFR 3.73(b) Statement (when there is an assignee) ☐ Power of Attorney
11. ☐ English Translation Document (if applicable)
12. ☒ Information Disclosure Statement (IDS)/PTO-1449 ☒ Copies of IDS Citations
13. ☐ Preliminary Amendment
14. ☒ Return Receipt Postcard (MPEP 503)  
(Should be specifically itemized)
15. ☐ Certified Copy of Priority Document(s)  
(if foreign priority is claimed)
16. ☐ Other: .....

17. If a CONTINUING APPLICATION, check appropriate box, and supply the requisite information below and in a preliminary amendment, or in an Application Data Sheet under 37 CFR 1.76:

☐ Continuation ☐ Divisional ☐ Continuation-in-part (CIP)

of prior application No. \_\_\_\_\_

Prior application information:

Examiner \_\_\_\_\_

Group / Art Unit. \_\_\_\_\_

For CONTINUATION OR DIVISIONAL APPS only: The entire disclosure of the prior application, from which an oath or declaration is supplied under Box 5b, is considered a part of the disclosure of the accompanying continuation or divisional application and is hereby incorporated by reference. The incorporation can only be relied upon when a portion has been inadvertently omitted from the submitted application parts.

## 18. CORRESPONDENCE ADDRESS

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or ☒ Correspondence address below

Name	William W. Haefliger				
Address	201 So. Lake Ave., Suite 512				
City	Pasadena	State	CA	Zip Code	91101
Country	U.S.A.	Telephone	(323) 684-2707	Fax	(626) 449-0520

Name (Print/Type)	William W. Haefliger	Registration No. (Attorney/Agent)	17,120
Signature			Date 11-8-00

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Application Number	
Filing Date	
First Named Inventor	David W. Warren et al
Examiner Name	
Group Art Unit	
Attorney Docket No.	12,150

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Large Entity Fee Code (\$)	Small Entity Fee Code (\$)	Fee Description	Fee Paid
101 710	201 355	Utility filing fee	355.
106 320	206 160	Design filing fee	
107 490	207 245	Plant filing fee	
108 710	208 355	Reissue filing fee	
114 150	214 75	Provisional filing fee	

**SUBTOTAL (1)** (\$ 355.**2. EXTRA CLAIM FEES**

Total Claims	Extra Claims	Fee from below	Fee Paid
14	-20** =	X	
1	-3** =	X	
Multiple Dependent			

Large Entity Fee Code (\$)	Small Entity Fee Code (\$)	Fee Description
103 18	203 9	Claims in excess of 20
102 80	202 40	Independent claims in excess of 3
104 270	204 135	Multiple dependent claim, if not paid
109 80	209 40	** Reissue independent claims over original patent
110 18	210 9	** Reissue claims in excess of 20 and over original patent

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**FEE CALCULATION (continued)****3. ADDITIONAL FEES**

Large Entity Fee Code (\$)	Small Entity Fee Code (\$)	Fee Description	Fee Paid
105 130	205 65	Surcharge - late filing fee or oath	
127 50	227 25	Surcharge - late provisional filing fee or cover sheet	
139 130	139 130	Non-English specification	
147 2,520	147 2,520	For filing a request for ex parte reexamination	
112 920*	112 920*	Requesting publication of SIR prior to Examiner action	
113 1,840*	113 1,840*	Requesting publication of SIR after Examiner action	
115 110	215 55	Extension for reply within first month	
116 390	216 195	Extension for reply within second month	
117 890	217 445	Extension for reply within third month	
118 1,390	218 695	Extension for reply within fourth month	
128 1,890	228 945	Extension for reply within fifth month	
119 310	219 155	Notice of Appeal	
120 310	220 155	Filing a brief in support of an appeal	
121 270	221 135	Request for oral hearing	
138 1,510	138 1,510	Petition to institute a public use proceeding	
140 110	240 55	Petition to revive - unavoidable	
141 1,240	241 620	Petition to revive - unintentional	
142 1,240	242 620	Utility issue fee (or reissue)	
143 440	243 220	Design issue fee	
144 600	244 300	Plant issue fee	
122 130	122 130	Petitions to the Commissioner	
123 50	123 50	Petitions related to provisional applications	
126 240	126 240	Submission of Information Disclosure Stmt	
581 40	581 40	Recording each patent assignment per property (times number of properties)	40.
146 710	246 355	Filing a submission after final rejection (37 CFR § 1.129(a))	
149 710	249 355	For each additional invention to be examined (37 CFR § 1.129(b))	
179 710	279 355	Request for Continued Examination (RCE)	
169 900	169 900	Request for expedited examination of a design application	

Other fee (specify) \_\_\_\_\_

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**SUBTOTAL (3)** (\$ 40.**SUBMITTED BY**

Name (Print/Type) William W. Haefliger

Registration No. (Attorney/Agent)

17,120

Complete (if applicable)

Telephone (323) 684-2707

Signature

Date

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1 TO WHOM IT MAY CONCERN:

2

3 BE IT KNOWN THAT WE, DAVID W. WARREN, a  
4 citizen of the United States of America, residing in  
5 Van Nuys, in the County of Los Angeles, and MICHAEL B.  
6 DONAHUE, a citizen of the United States of America,  
7 residing in La Verne, in the County of Los Angeles,  
8 both in the State of California, have invented a new  
9 and useful improvement in

10

11

12 **THERMALLY-INTEGRATED LOW TEMPERATURE WATER-GAS SHIFT**

13 **REACTOR APPARATUS AND PROCESS**

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1                   **BACKGROUND OF THE INVENTION**

2  
3                   This invention relates to a process and an  
4 apparatus for producing hydrogen for application to  
5 fuel cell electric generators.

6                   Catalytic reaction apparatus and processes  
7 for converting hydrocarbon feedstocks to useful  
8 industrial gases, such as hydrogen, is well known in  
9 the art. Proton exchange membrane (PEM) fuel cells  
10 have emerged as a viable option for the production of  
11 disbursed electrical power, typically in the range of  
12 2-50 k W, for use in residential and small commercial  
13 applications. PEM fuel cells generate electricity by  
14 the electrochemical reaction between hydrogen and  
15 oxygen.

16                  While oxygen is readily available from  
17 ambient air, hydrogen must be produced from  
18 commercially available fuels, such a natural gas or  
19 propane, using methods such as steam reforming. Steam  
20 reforming is a process that involves a high temperature  
21 catalytic reaction between a hydrocarbon and steam to  
22 form a hydrogen-rich product gas, commonly referred to  
23 as reformat, that contains significant quantities of  
24 carbon monoxide.

1            Since PEM fuel cells have a low tolerance to  
2 carbon monoxide, the concentration of carbon monoxide  
3 in the reformat must be reduced using a catalytic  
4 reaction step known as the water-gas shift reaction.  
5 Following the water-gas shift reaction, the  
6 concentration of carbon monoxide in the reformat is  
7 further reduced to concentrations typically less than  
8 10 ppm using a selective oxidation reaction, also  
9 referred to as preferential oxidation or PROX. The  
10 combination of processes that convert commercial fuels  
11 to a reformat suitable for use in a fuel cell is  
12 commonly referred to as a fuel processor.

13            As an illustration, Table 1 summarizes the  
14 reaction steps of a fuel processor designed to produce  
15 a hydrogen-rich gas stream suitable for use in a PEM  
16 fuel cell.

17  
18            Table 1. PEM fuel processor reaction steps

19

20	1. $\text{CH}_4 + \text{H}_2\text{O} = \text{CO} + \text{H}_2$	Steam reforming
21	2. $\text{CO} + \text{H}_2\text{O} = \text{CO}_2 + \text{H}_2$	Water-gas shift
22	3. $\text{CO} + \frac{1}{2}\text{O}_2 = \text{CO}_2$	Selective oxidation

23

24            In typical industrial practice, the water-gas  
25 shift reaction is conducted in two separate adiabatic  
26 reactors operating at two different temperature

1 regimes. The first reactor, known as the high  
2 temperature shift reactor, operates at inlet  
3 temperatures typically ranging from about 550°F to  
4 650°F. The second reactor, known as the low  
5 temperature shift reactor, operates at an inlet  
6 temperature typically ranging from about 380°F to  
7 450°F. The combination of the two sequential water-gas  
8 shift reactions typically reduces the concentration of  
9 carbon monoxide in the reformat to less than 1.0  
10 volume percent.

11           The use of a low temperature shift reactor is  
12 beneficial because the water-gas shift reaction is  
13 thermodynamically favored at lower temperatures.  
14 However, a high temperature shift reactor is generally  
15 required to limit the amount of heat that is released  
16 in the low temperature shift reactor.

17           Conventional low temperature shift catalysts  
18 comprise a mixture of copper and zinc that are  
19 supported on a ceramic carrier. These catalysts  
20 promote the water-gas shift reaction at lower  
21 temperature, but lose activity if they are exposed to  
22 excessively high temperatures due to sintering of the  
23 active metals. Therefore, it is generally desirable to  
24 limit the maximum temperature of the low temperature  
25 shift catalyst to about 500°F in order to achieve long  
26 catalyst life.

1           The water-gas shift reaction releases  
2 approximately 9837 calories per gram-mole of carbon  
3 monoxide that is consumed. If the water-gas shift  
4 reaction were conducted using a single adiabatic low  
5 temperature shift reactor, the heat release would  
6 result in a temperature increase across the catalyst  
7 bed that would exceed the desirable temperature limit  
8 for conventional low temperature shift reactors.  
9 Furthermore, the high exit temperature from the water-  
10 gas shift reactor would be thermodynamically less  
11 favorable for achieving high conversions of carbon  
12 monoxide.

13           There is need to minimize the number of  
14 reactors and heat exchangers that are needed to achieve  
15 the objective of high conversion of carbon monoxide for  
16 PEM fuel cell applications, in order to reduce the  
17 size, cost and complexity of the fuel processor.  
18 Therefore, it is desirable to conduct the water-gas  
19 shift reaction using a single reactor vessel that is  
20 maintained within acceptable operating temperature  
21 limits by controlling heat removal from the reactor.

22           The steam reforming reaction requires large  
23 quantities of steam for the conversion of hydrocarbon  
24 to reformat. It is desirable to recover the heat  
25 released from the water-gas shift reaction for the  
26 purpose of generating steam in order to improve the

1 thermal efficiency of the fuel processor. The present  
2 invention achieves the objective of temperature control  
3 and heat recovery by integrating a lower temperature  
4 shift reactor within a steam generator that contains  
5 water boiling at a temperature range of about 360°F to  
6 400°F, corresponding to a boiler pressure of about 153  
7 psia to 247 psia.

8           Because the vessel walls of the lower  
9 temperature shift reactor are in heat transfer  
10 communication with boiling water, the heat released  
11 from the water-gas shift reaction is effectively  
12 removed to control the temperature in the catalyst bed  
13 within the desired operating temperature range.  
14 Furthermore, the heat released from the water-gas shift  
15 reaction is beneficially recovered to generate steam  
16 that is used in the process. Finally, the steam  
17 generator provides a convenient source of heat for  
18 heating the catalyst bed during start-up.

19           U.S. Patent 6,086,840 describes a process for  
20 making ammonia that mentions use of an isothermal shift  
21 reactor that includes heat exchange tubes extending  
22 within a vessel packed with catalyst. The heat  
23 exchange tubes contain a boiling fluid to remove heat  
24 from the catalyst bed.

25



1                                   **SUMMARY OF THE INVENTION**

2

3                   It is the general object of this invention to  
4 provide a novel catalytic reaction apparatus and  
5 process for the reduction of carbon monoxide contained  
6 in hydrogen-rich gas streams, employing lower  
7 temperature shift reactor that is in thermal  
8 communication with a steam generator operating in a  
9 temperature range that is optimum for catalytic  
10 activity and thermodynamic conversion, and allows the  
11 recovery of useful waste heat to generate steam needed  
12 for a process to convert hydrocarbons feedstocks to  
13 useful gases, such as hydrogen. The subject invention  
14 is particularly well suited for the production of  
15 hydrogen for fuel cells having low tolerance to carbon  
16 monoxide.

17                   Basically, the invention provides a  
18 thermally-integrated low temperature water-gas shift  
19 reactor for converting carbon monoxide in the presence  
20 of steam to form carbon dioxide and water comprising,  
21 in combination,

22                   a) a waste-heat recovery steam generator  
23 for the beneficial recovery of exothermic reaction heat  
24 to generate steam that is used in a process for the

1 conversion of hydrocarbon feedstock into hydrogen-rich  
2 gases,

3           b) an outer annulus extending about said  
4 waste-heat steam generator,

5           c) a catalyst bed located within said outer  
6 region, and through which reformat gases flow,

7           d) the outer region being in heat transfer  
8 communication with the steam generator to maintain the  
9 catalyst bed within a predetermined temperature range  
10 for operation of a low temperature shift reaction.

11           These and other objects and advantages of the  
12 invention, as well as the details of an illustrative  
13 embodiment, will be more fully understood from the  
14 following specification and drawings, in which:

15

16                           **DRAWING DESCRIPTION**

17

18           Fig. 1 is a flow diagram of a process that  
19 incorporates a thermally-integrated low temperature  
20 water-gas shift reactor;

21           Fig. 2 is a schematic showing of apparatus  
22 for testing a thermally-integrated low temperature  
23 water-gas shift apparatus;

1           Fig. 3a is a schematic showing of a  
2 thermally-integrated low temperature water-gas shift  
3 reactor apparatus;

4           Fig. 3b is a section taken on lines 3b-3b of  
5 Fig. 3a; and

6           Fig. 4 is a schematic showing of an alternate  
7 thermally-integrated low temperature water-gas shift  
8 reactor apparatus.

9

## 10                           **DETAILED DESCRIPTION**

11

### 12           PROCESS AND APPARATUS

13

14           The process and apparatus as shown in Fig. 1  
15 controls the temperature of a low temperature shift  
16 reactor and makes beneficial use of the heat of  
17 reaction to generate steam that is employed to produce  
18 hydrogen-rich gases containing low concentrations of  
19 carbon monoxide from hydrocarbon feedstocks.

20           A reactant mixture at 1 consists of  
21 hydrocarbon feedstock 32 and steam 11. The mixture is  
22 preheated in an exchanger 2 and introduced into a  
23 tubular catalytic reactor 3 that is contained within a  
24 combustion chamber 4. The tubular catalytic reactor  
25 typically contains a supported Ni catalyst and is

1 commonly referred to in the industry as a steam  
2 reformer. Fuel 5 and air 6 are combusted in the  
3 chamber 4 to heat the reactant mixture so as to produce  
4 a hydrogen-rich stream 7 containing carbon monoxide  
5 concentrations typically ranging from 5% to 15%.

6 Combustion products 8 from the combustion  
7 chamber pass through a flue gas heat exchange coil 9  
8 that is contained within a waste heat steam generator  
9 10, wherein the combustion products are cooled and steam  
10 11 is generated. The cooled combustion products 13 are  
11 further cooled by exchanging heat in a feed water  
12 exchanger 14 that produces heated water 15 that is  
13 supplied to the waste heat steam generator 10.

14 The hydrogen-rich stream 7 from the tubular  
15 catalytic reactor 3 is cooled in an exchanger 2 to a  
16 temperature typically in the range of 400°F-550°F  
17 whereupon the cooled steam 18 is introduced into a  
18 fixed-bed catalytic reactor 19 shown as surrounding  
19 steam generator 10, to effect a water gas shift  
20 reaction that converts a portion of the carbon monoxide  
21 to hydrogen and carbon dioxide by reaction with steam.  
22 The catalyst bed reactor typically contains a supported  
23 Cu/Zn catalyst and is commonly known in the industry as  
24 a low temperature shift reactor. The walls 20 of the  
25 low temperature shift reactor are in thermal  
26 communication with boiling water contained in the waste

1 heat steam generator. The heat released in the low  
2 temperature shift reactor is thus beneficially  
3 recovered to generate steam. The carbon monoxide  
4 concentration of the process gas 21 exiting the low  
5 temperature shift reactor is typically less than 0.5%.

6 The products from the low temperature shift  
7 reactor are cooled in a process exchange coil 22 to  
8 condense moisture. The condensed moisture 40a is  
9 separated in a separator vessel 28 and is pumped at 40b  
10 to heat exchanger 14 using pump 41. Make-up water may  
11 be added as at 40c. The cooled process gas 29 is mixed  
12 with a small quantity of air 30 and is sent to the  
13 selective oxidizer reactor 31. The required quantity  
14 of ambient air that must be introduced into the process  
15 gas depends on the specific performance of the catalyst  
16 but typically ranges from 2 to 4 times the quantity  
17 necessary to provide a stoichiometric quantity oxygen  
18 for the complete oxidation of carbon monoxide.

19 The process gas 32 exiting the selective  
20 oxidizer typically contains less than 10 ppm carbon  
21 monoxide and is available for use, for instance, in  
22 fuel cells having a low tolerance to carbon monoxide.  
23 A fuel cell is indicated at 100.

24  
25  
26

## 1 EXPERIMENTAL DATA

2

3 Tests were conducted to measure the  
4 conversion of carbon monoxide contained in a simulated  
5 reformat gas stream that was passed over a commercial  
6 Cu/Zn catalyst. The Cu/Zn catalyst was contained  
7 within tubular conduit walls that were in thermal  
8 communication with a boiling water fluid. The  
9 objective of the tests was to quantify the relation  
10 between CO conversion and catalyst gas hourly space  
11 velocity (GHSV) as a function of the temperature of the  
12 boiling water fluid.

13 The experimental test system is shown in Fig.  
14 2. The Cu/Zn catalyst 80 was packed in a  $\frac{3}{4}$  inch tube  
15 81 that was surrounded by a metallic water jacket 82.  
16 Steam 83 generated from the water jacket was sent to a  
17 condenser 84 and the condensed liquid 85 was returned  
18 to the water jacket by natural circulation. An  
19 electrical heater 86 was placed on the outer surface of  
20 the jacket and a temperature controller 87 was used to  
21 control the heat input in order to maintain the water  
22 jacket at the desired temperature. A simulated  
23 reformat gas mixture 88 was heated in a pre-heater 89  
24 to a temperature approximately equal to the boiling  
25 water fluid temperature before the gases entered the  
26 catalyst bed. The product gases 90 at the exit of the

1 catalyst bed were cooled, condensed and sent to a gas  
2 chromatograph for compositional analysis. Table 2  
3 summarizes the results for tests conducted using the  
4 experimental apparatus.

5

6 Table 2. Carbon Monoxide exit concentration as a  
7 function of boiler temperature and catalyst space  
8 velocity

9

10 Simulated Reformate Composition at Inlet to Reactor:

11

12		Wet Gas	Dry Gas
13	<u>Component</u>	<u>Vol. %</u>	<u>Vol. %</u>
14	CO	5.70	10.0
15	CO <sub>2</sub>	8.55	15.0
16	H <sub>2</sub>	39.90	70.0
17	CH <sub>4</sub>	2.85	5.0
18	H <sub>2</sub> O	43.00	0.0
19			
20	Total	100.00	100.0

21

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	<u>Dry Gas</u> <u>GHSV (hr-1)</u>	<u>Boiler</u> <u>Temperature°F</u>	<u>Carbon Monoxide</u> <u>Exit Concentration</u> <u>(Vol.% dry gas)</u>
4	1930	340	3.67
5	762	340	0.62
6	2950	385	2.84
7	2440	385	2.08
8	1930	385	1.70
9	1425	385	0.90
10	1930	398	1.08
11	1425	398	0.55

In order to maximize hydrogen yield and minimize the quantity of carbon monoxide that must be converted in the selective oxidizer, it is generally desirable to achieve less than 1.0 vol.% CO in the dry gas at the exit of the shift reactor. It is desirable to operate at the maximum space velocity in order to minimize the size of the catalyst bed.

The results show that when the boiler is maintained at temperatures above about 385°F, the CO concentration is less than about 1.0 vol.% (dry gas) for space velocities less than or equal to about 1500hr-1. Higher space velocities can be achieved for even higher boiler temperatures, however this necessitates operation at pressures above 250 psig,



1 which may not be desirable for many PEM fuel cell  
2 applications.

3           The results indicate that there is an optimum  
4 temperature range of operation for the boiler that  
5 achieves the objects of minimum catalyst volume,  
6 moderate boiler pressure and low CO concentration at  
7 the shift reactor exit. This optimum temperature range  
8 is approximately 385°F to 400°F.

9  
10       THERMALLY-INTEGRATED LOW TEMPERATURE WATER-GAS SHIFT  
11                           REACTOR APPARATUS

12  
13           Apparatus shown in Figs. 3a and 3b controls  
14 the temperature of a low temperature shift reactor and  
15 makes beneficial use of the heat of reaction to  
16 generate steam.

17           In the preferred embodiment, the apparatus  
18 comprises an annular catalyst zone 50 within vessel 50a  
19 that is concentrically disposed around an inner steam  
20 generator zone 51 within vessel 51a. The catalyst zone  
21 contains a lower temperature shift catalyst, typically  
22 comprising a catalytically active mixture of copper and  
23 zinc metals, that promote the water-gas shift reaction  
24 at temperatures typically in the range of 370°F to  
25 500°F. The catalyst zone is defined by the annular  
26 space between an outer wall 52 and an inner wall 53.

1 The steam generator zone is defined in the space inside  
2 of the inner wall, a top wall 65, and a tube sheet 66.

3 Reformate containing carbon monoxide enters  
4 an inlet conduit 54 that is in communication with the  
5 annular catalyst zone. The reformate passes through  
6 the catalyst zone, releasing heat due to the exothermic  
7 nature of the water-gas shift reaction. The reformate  
8 exits from the catalyst zone through an exit conduit  
9 55.

10 The inner wall 53 is in thermal contact with  
11 the reformate gases flowing through the catalyst zone  
12 and boiling water 56 contained in the steam generator  
13 zone, the catalyst zone shown as surrounding the steam  
14 generation zone. This results in a transfer of heat  
15 from the catalyst zone to the steam generator zone in  
16 order to maintain the catalyst zone within a defined  
17 temperature range that is optimum for conducting the  
18 low temperature shift reaction.

19 The steam generator zone contains a heat  
20 transfer conduit 57, or a multitude of heat transfer  
21 conduits, that is immersed within the boiling water.  
22 The heat transfer conduit conveys hot combustion  
23 products, such as from the combustion section of a  
24 steam reformer, to transfer heat to the boiling water  
25 for the purpose of generating steam. The hot  
26 combustion products enter an inlet plenum 58 through an

1 inlet conduit 59. The inlet plenum is in communication  
2 with the inlet portion 60 of the heat transfer conduit.  
3 The hot combustion products exit the heat transfer  
4 conduit to an exit plenum 61 that is connected to an  
5 exit conduit 62. Steam that is generated from the heat  
6 transferred to the steam generator zone through the  
7 inner wall 53 and the heat transfer conduit 57 exits  
8 the steam generator zone through an exit conduit 68.  
9 Water is fed to the steam generator zone through an  
10 inlet conduit 69 to maintain the boiling water at a  
11 desired level that is sufficient to efficiently remove  
12 heat from the inner wall and the heat transfer conduit.

13           The annular catalyst zone 50 may include  
14 means to enhance heat transfer between the catalyst bed  
15 and the inner wall 53 such as the use of longitudinal  
16 fins 70 that are attached to the inner wall and extend  
17 a distance into the annular catalyst space. Other heat  
18 transfer enhancements such as metal packing within the  
19 annular catalyst zone, or active catalyst that are  
20 incorporated into highly thermally conductive  
21 monoliths, may be beneficially used in the invention.

22

#### 23 EXAMPLE

24           A pipe wall having an outside diameter of 5.5  
25 inches defines a waste heat steam generator zone. The  
26 pipe wall is in thermal communication with an annular

1 catalyst zone that is concentrically disposed around  
2 the waste heat steam generator zone. The space between  
3 the 5.5 inch diameter pipe and an outer wall having an  
4 8 inch inside diameter define the annular catalyst  
5 zone. The annular catalyst zone is packed with 4.8 mm  
6 x 2.8 mm low temperature shift catalyst containing  
7 principally a mixture of Cu and Zn supported on a  
8 ceramic carrier. The packed height of the annular  
9 catalyst zone is approximately 12 inches and  
10 corresponds to the approximate height of the water  
11 contained within the waste heat steam generator zone.  
12 The total catalyst volume is approximately 0.184 cubic  
13 feet.

14           The waste heat steam generator zone also  
15 contains heat transfer conduits that are immersed  
16 within the boiling water. The heat transfer conduits  
17 consist of 5/8 inch diameter tubes that are formed in a  
18 u-tube arrangement having inlet means and exit means  
19 that are attached to a single tube sheet. Hot  
20 combustion products from a steam reformer are directed  
21 to the inlet means of the heat transfer tubes. Cooled  
22 combustion products are exhausted from the exit means  
23 of the heat transfer tubes.

24           The waste heat steam generator zone is  
25 operated at a controlled pressure using a back-pressure  
26 regulator that is located on the steam exit conduit.

1 The back-pressure regulator is set at a pressure of 220  
2 psia corresponding to a saturated water temperature of  
3 390°F.

4 Reformate from a tubular catalytic reactor is  
5 cooled to approximately 510°F and is introduced into  
6 the top of the annular catalyst zone. The reformate  
7 exits the bottom of the annular catalyst zone at a  
8 temperature of approximately 430°F. The composition  
9 and flow rate of the reformate at the inlet and exit of  
10 the annular catalyst zone is shown in Table 3.

11

12 Table 3. Gas composition from thermally-integrated low  
13 temperature water-gas shift reactor

14

15 Gas Composition (Volume %)  
16 Component Reformate Inlet Reformate Exit

17	CH <sub>4</sub>	2.1	2.1
18	CO	8.1	0.8
19	CO <sub>2</sub>	7.5	14.7
20	H <sub>2</sub>	52.6	59.8
21	H <sub>2</sub> O	29.7	22.5

22

23	Total	100.00	100.0
----	-------	--------	-------

24

25	Total Flow, SCFH	280	280
----	------------------	-----	-----

26	Temperature, °F	510	430
----	-----------------	-----	-----

27	Pressure, psia	16.7	16.7
----	----------------	------	------

1       ALTERNATIVE EMBODIMENT OF THERMALLY-INTEGRATED LOW  
2       TEMPERATURE WATER-GAS SHIFT REACTOR APPARATUS  
3

4               Fig. 4 depicts an alternative embodiment of  
5 the thermally-integrated low temperature water-gas  
6 shift reactor apparatus. A helical coil 75 is welded  
7 to the surfaces of the inner wall 53 and outer wall 52  
8 that define the annular catalyst space. The catalyst  
9 is packed within the volumes defined by the helical  
10 coil and the inner and outer walls. The gases entering  
11 the inlet conduit 54 are directed in a helical manner  
12 around the annular space by virtue of the confining  
13 helical coil. This increases the velocity of the gases  
14 within the catalyst bed for a given space velocity in  
15 order to enhance the rate of heat transfer to and from  
16 the bed. The helical coil also serves as an extended  
17 heat transfer surface to enhance the rate of heat  
18 transfer to and from the inner wall of the annular  
19 space. Elements the same as those of Fig. 3a bear the  
20 same identifying numbers.

1    WE CLAIM:

2

3            1.    A thermally-integrated low  
4    temperature water-gas shift reactor for converting  
5    carbon monoxide in the presence of steam to form carbon  
6    dioxide and water comprising, in combination,

7            a)    a waste-heat recovery steam generator  
8    for the beneficial recovery of exothermic reaction heat  
9    to generate steam that is used in a process for the  
10   conversion of hydrocarbon feedstock into hydrogen-rich  
11   gases,

12           b)    an outer region extending about said  
13   waste-heat steam generator,

14           c)    a catalyst bed located within said outer  
15   region, and through which reformat gases flow,

16           d)    the outer region being in heat transfer  
17   communication with the steam generator to maintain the  
18   catalyst bed within a predetermined temperature range  
19   for operation of a low temperature shift reaction.

20

21

22

23

24

25

1           2.    The combination of claim 1 wherein the  
2 waste heat steam generator operates at temperatures in  
3 one of the following ranges: 360°F to 450°F, and of  
4 385°F to 400°F, that is optimum for conducting the low  
5 temperature water-gas shift reaction.

6  
7  
8           3.    The combination of claim 1 wherein a  
9 Cu/Zn catalyst is contained in an annular space defined  
10 by said outer region, and having an inner wall that is  
11 in thermal contact with a boiling water fluid in said  
12 generator.

13  
14  
15           4.    The combination of claim 3 wherein the  
16 boiling water fluid is located to transfer heat to the  
17 catalyst bed to heat the bed during start-up.

18  
19  
20           5.    The combination of claim 3 wherein the  
21 catalyst bed is located to transfer heat to the boiling  
22 water fluid during normal operation to generate steam.

23  
24  
25  
26



1           6.    The combination of claim 1 including  
2 longitudinal heat transfer fins attached to an inside  
3 wall of the annulus and projecting in said bed to  
4 enhance the rate of heat transfer to and from the  
5 catalyst bed.

6  
7  
8           7.    The combination of claim 1 including a  
9 helical coil adjacent the inner and outer walls for  
10 defining annular space at said annulus to conduct and  
11 increase the velocity of the process gases as they flow  
12 through the catalyst bed and to enhance the rate of  
13 heat transfer to and from the catalyst bed.

14  
15  
16           8.    The combination of claim 1 wherein the  
17 catalyst bed is maintained in one of the following  
18 ranges:   between 370°F and 550°F, and between 400°F and  
19 450°F.

20  
21  
22           9.    The combination of claim 3 wherein the  
23 annular space is typically between 1 and 2 inches wide  
24 to minimize temperature differentials between the  
25 outside and inside walls defined by the annular space.

26

1           10. The combination of claim 3 wherein the  
2 gas has hourly space velocity in the range of 500hr-1  
3 to 2000hr-1.

4  
5  
6           11. The combination of claim 1 wherein the  
7 waste heat stem generator contains one or more heat  
8 transfer conduits that transfer heat from hot  
9 combustion products to a boiling water fluid for the  
10 purpose of generating steam.

11  
12  
13           12. The combination of claim 1 wherein the  
14 steam generator includes an upright vessel, said outer  
15 region having an upper level inlet flowing reformat  
16 into the catalyst bed, the reformat containing carbon  
17 monoxide, and said region having a lower level outlet,  
18 a catalyst bed located between said upper and lower  
19 levels, a heat transfer conduit or conduits extending  
20 within said vessel and immersed within boiling water  
21 contained in said vessel inwardly of said catalyst bed,  
22 said conduit or conduits receiving hot products of  
23 combustion from a combustion process, for transfer of  
24 heat to the boiling water, for generating steam exiting  
25 from said vessel.

26

1           13. The combination of claim 1 wherein the  
2 catalyst bed extends helically about said generator.

3

4

5           14. The combination of claim 1 including a  
6 helical coil in said outer region and extending about  
7 said generator, to direct said reformat gases  
8 helically and through said catalyst bed, to enhance  
9 heat transfer via said bed.

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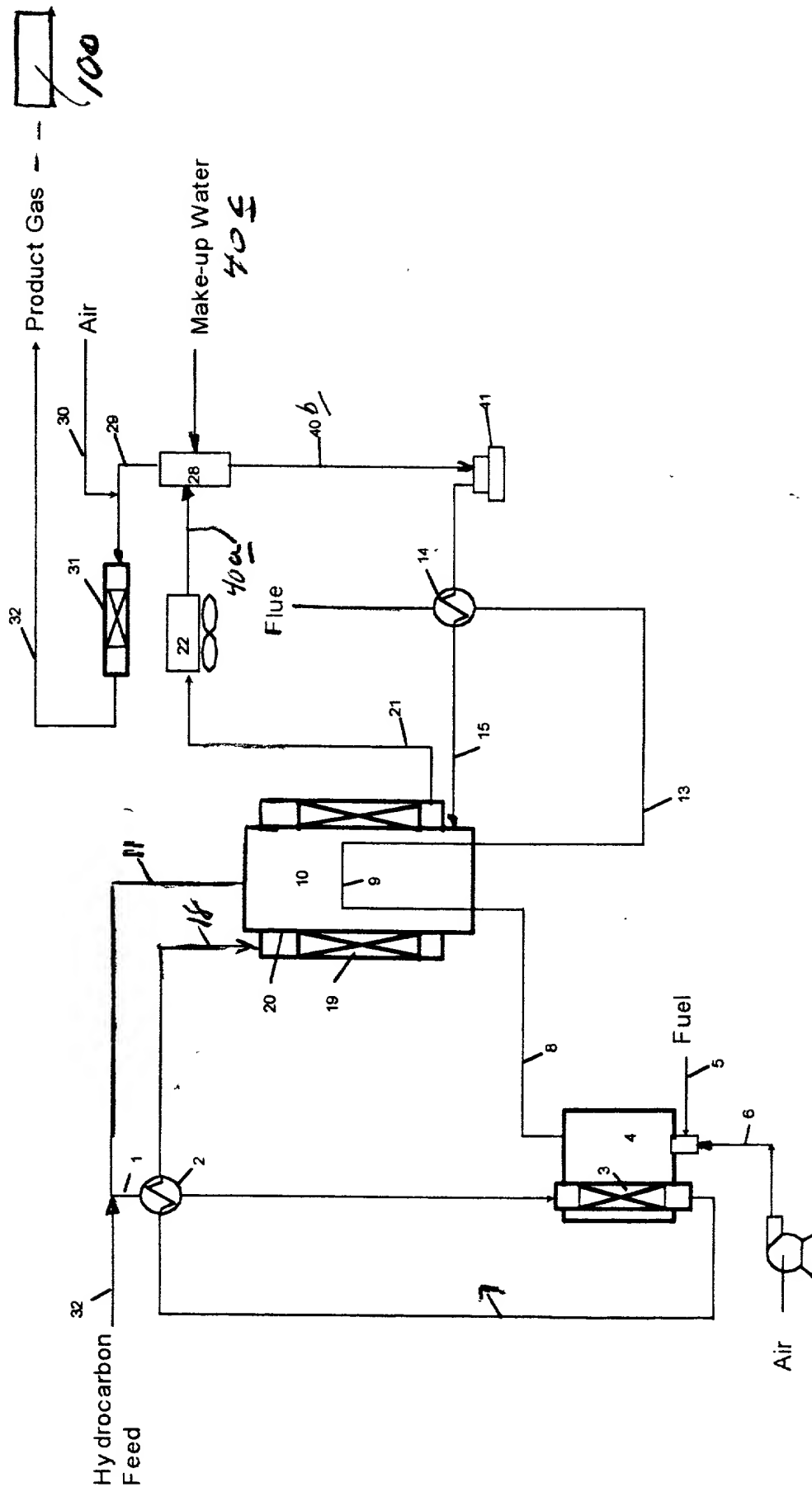
1                   **ABSTRACT OF THE DISCLOSURE**

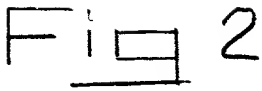
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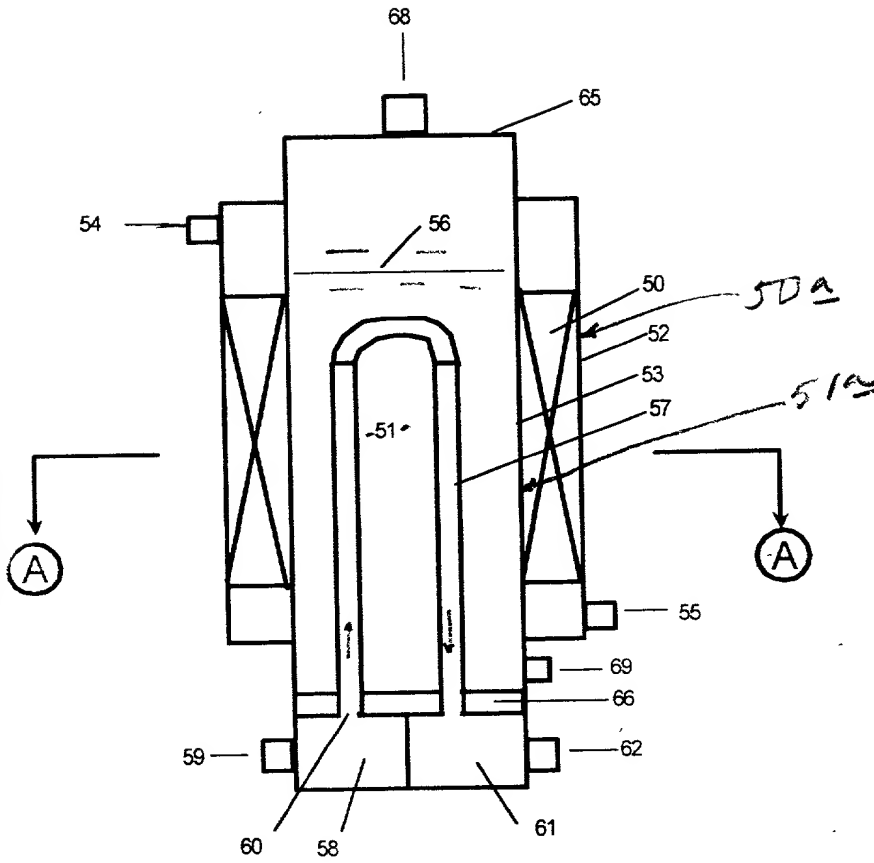
3                   A thermally-integrated lower temperature  
4   water-gas shift reactor apparatus for converting carbon  
5   monoxide in the presence steam comprises a catalyst bed  
6   that is disposed within an outer region surrounding a  
7   waste heat recovery steam generator operating at a  
8   selected pressure corresponding to the optimum  
9   temperature for conducting the catalytic water-gas  
10  shift reaction and a process for useful recovery of the  
11  exothermic heat of reaction to generate steam that is  
12  used in a process for the conversion of hydrocarbon  
13  feedstock into useful gases such as hydrogen.

14

12,150  
1 of 4

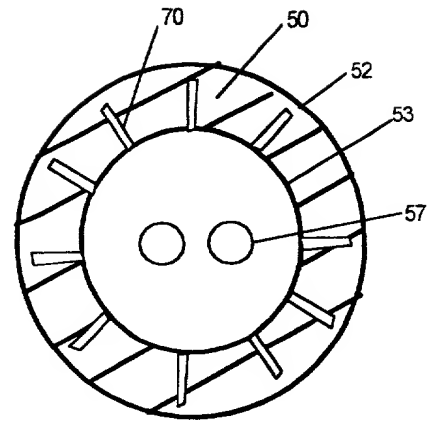


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SIDE VIEW

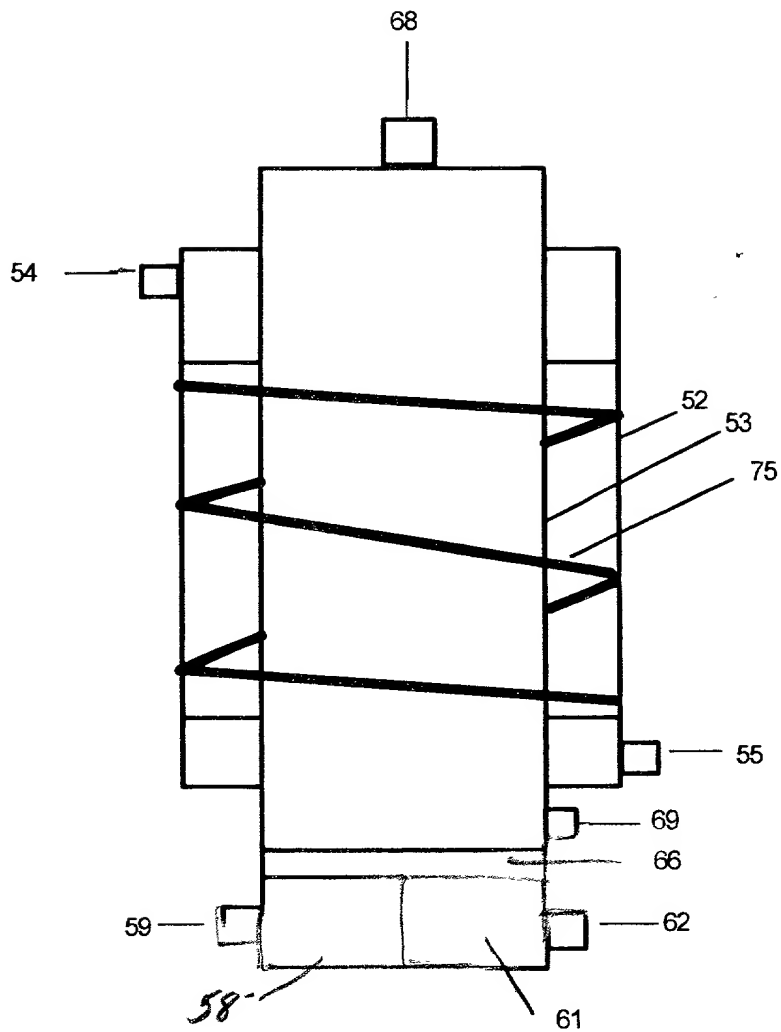
(a)



SECTION A

(b)

Fig 3



SIDE VIEW

Fig 4



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**DECLARATION FOR UTILITY OR  
DESIGN  
PATENT APPLICATION  
(37 CFR 1.63)**

☒ Declaration Submitted with Initial Filing **OR** ☐ Declaration Submitted after Initial Filing (surcharge (37 CFR 1.16 (e)) required)

Attorney Docket Number	12,150
First Named Inventor	David W. Warren
<b>COMPLETE IF KNOWN</b>	
Application Number	/
Filing Date	
Group Art Unit	
Examiner Name	

As a below named inventor, I hereby declare that:

My residence, post office address, and citizenship are as stated below next to my name.

I believe I am the original, first and sole inventor (if only one name is listed below) or an original, first and joint inventor (if plural names are listed below) of the subject matter which is claimed and for which a patent is sought on the invention entitled:

**THERMALLY-INTEGRATED LOW TEMPERATURE WATER-GAS  
SHIFT REACTOR APPARATUS AND PROCESS**

the specification of which (Title of the Invention)

☒ is attached hereto

OR

☐ was filed on (MM/DD/YYYY) as United States Application Number or PCT International

Application Number and was amended on (MM/DD/YYYY) (if applicable).

I hereby state that I have reviewed and understand the contents of the above identified specification, including the claims, as amended by any amendment specifically referred to above.

I acknowledge the duty to disclose information which is material to patentability as defined in 37 CFR 1.56.

I hereby claim foreign priority benefits under 35 U.S.C. 119(a)-(d) or 365(b) of any foreign application(s) for patent or inventor's certificate, or 365(a) of any PCT international application which designated at least one country other than the United States of America, listed below and have also identified below, by checking the box, any foreign application for patent or inventor's certificate, or of any PCT international application having a filing date before that of the application on which priority is claimed.

Prior Foreign Application Number(s)	Country	Foreign Filing Date (MM/DD/YYYY)	Priority Not Claimed	Certified Copy Attached?	
				YES	NO
			<input type="checkbox"/>	<input type="checkbox"/>	<input type="checkbox"/>
			<input type="checkbox"/>	<input type="checkbox"/>	<input type="checkbox"/>
			<input type="checkbox"/>	<input type="checkbox"/>	<input type="checkbox"/>
			<input type="checkbox"/>	<input type="checkbox"/>	<input type="checkbox"/>

☐ Additional foreign application numbers are listed on a supplemental priority data sheet PTO/SB/02B attached hereto:

I hereby claim the benefit under 35 U.S.C. 119(e) of any United States provisional application(s) listed below.

Application Number(s)	Filing Date (MM/DD/YYYY)	<input type="checkbox"/> Additional provisional application numbers are listed on a supplemental priority data sheet PTO/SB/02B attached hereto.

[Page 1 of 2]

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## DECLARATION — Utility or Design Patent Application

I hereby claim the benefit under 35 U.S.C. 120 of any United States application(s), or 365(c) of any PCT international application designating the United States of America, listed below and, insofar as the subject matter of each of the claims of this application is not disclosed in the prior United States or PCT International application in the manner provided by the first paragraph of 35 U.S.C. 112, I acknowledge the duty to disclose information which is material to patentability as defined in 37 CFR 1.56 which became available between the filing date of the prior application and the national or PCT international filing date of this application.

U.S. Parent Application or PCT Parent Number	Parent Filing Date (MM/DD/YYYY)	Parent Patent Number (if applicable)

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As a named inventor, I hereby appoint the following registered practitioner(s) to prosecute this application and to transact all business in the Patent and Trademark Office connected therewith:

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Name	Registration Number	Name	Registration Number
William W. Haefliger	17,120		

☐ Additional registered practitioner(s) named on supplemental Registered Practitioner Information sheet PTO/SB/02C attached hereto.

Direct all correspondence to: ☐ Customer Number or Bar Code Label ☒ Correspondence address below

Name	William W. Haefliger				
Address	201 So. Lake Ave., Suite 512				
Address					
City	Pasadena	State	CA	ZIP	91101
Country	U.S.A.	Telephone	(323) 684-2707	Fax	(626) 449-0520

I hereby declare that all statements made herein of my own knowledge are true and that all statements made on information and belief are believed to be true; and further that these statements were made with the knowledge that willful false statements and the like so made are punishable by fine or imprisonment, or both, under 18 U.S.C. 1001 and that such willful false statements may jeopardize the validity of the application or any patent issued thereon.

Name of Sole or First Inventor:		<input type="checkbox"/> A petition has been filed for this unsigned inventor			
Given Name (first and middle (if any))		Family Name or Surname			
David W.		Warren			
Inventor's Signature	<i>David W. Warren</i>			Date	11/1/00
Residence: City	Van Nuys	State	CA	Country	U.S.A.
Post Office Address	5702 Colbath Avenue				
Post Office Address					
City	Van Nuys	State	CA	ZIP	91401
Country	U.S.A.				

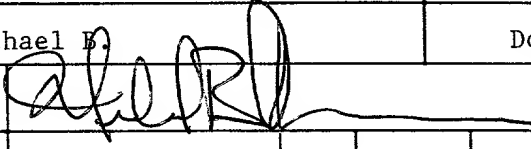
☒ Additional inventors are being named on the supplemental Additional Inventor(s) sheet(s) PTO/SB/02A attached hereto

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+

## DECLARATION

ADDITIONAL INVENTOR(S)  
Supplemental Sheet  
Page 3 of 3

<b>Name of Additional Joint Inventor, if any:</b>				<input type="checkbox"/> A petition has been filed for this unsigned inventor			
Given Name (first and middle [if any])				Family Name or Surname			
Michael B.				Donahue			
Inventor's Signature						Date	
Residence: City			State		Country		Citizenship
La Verne			CA		U.S.A.		U.S.A.
Post Office Address							
2515 Galicia							
Post Office Address							
City		State		ZIP		Country	
La Verne		CA		91750		U.S.A.	
<b>Name of Additional Joint Inventor, if any:</b>				<input type="checkbox"/> A petition has been filed for this unsigned inventor			
Given Name (first and middle [if any])				Family Name or Surname			
Inventor's Signature						Date	
Residence: City			State		Country		Citizenship
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Given Name (first and middle [if any])				Family Name or Surname			
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